Bernoulli's Equation

- It states that the sum of kinetic, potential and pressure heads of a fluid particle is constant along a streamline during steady flow when compressibility and frictional effects are negligible.
- i.e., For an ideal fluid, Total head of fluid particle remains constant during a steady-incompressible flow.
- Or total head along a streamline is constant during steady flow when compressibility and frictional effects are negligible.

Total Head =
$$Z + \frac{P}{\gamma} + \frac{V^2}{2g} = constt$$

 $Z_1 + \frac{P_1}{\gamma} + \frac{V^2_1}{2g} = Z_2 + \frac{P_2}{\gamma} + \frac{V^2_2}{2g}$
 $H_1 = H_2$

Derivation of Bernoulli's Equation

- Consider motion of flow fluid particle in steady flow field as shown in fig.
- Applying Newton's 2nd Law in sdirection on a particle moving along a streamline give

$$F_s = ma_s$$
 Eq(I)

Where F is resultant force in sdirection, m is the mass and a_s is the acceleration along s-direction.

$$a_s = \frac{dV}{dt} = \frac{dsdV}{dsdt} = \frac{dsdV}{dtds} = V\frac{dV}{ds}$$
 Eq(2)

Assumption:

Fluid is ideal and incompressible Flow is steady Flow is along streamline Velocity is uniform across the section and is equal to mean velocity Only gravity and pressure forces are acting



Fig. Forces acting on particle along streamline

7

Derivation of Bernoulli's Equation

$$F_s = PdA - (P + dp)dA - W\sin\theta \quad \text{Eq(3)}$$

Substituting values from Eq(2) and Eq(3) to Eq(1)

$$PdA - (P + dp)dA - W\sin\theta = mV\frac{dV}{ds}$$

$$-dpdA - \rho g dA ds \frac{dz}{ds} = \rho dA ds V \frac{dV}{ds}$$

Cancelling dA and simplifying

8

$$-dp - \rho g dz = \rho V dV \qquad Eq(4)$$

Note that
$$VdV = \frac{1}{2}dV^2$$

 $-dp - \rho gdz = \rho \frac{1}{2}dV^2$ Eq(5)

Fig. Forces acting on particle along streamline

W=weight of fluid $W = mg = (\rho dAds)g$ Wsin(θ)= component acting along s-direction dA= Area of flow ds=length between sections along pipe

Derivation of Bernoulli's Equation

• Dividing eq (5) by ρ

$$\frac{dp}{\rho} + gdz + \frac{1}{2}dV^2 = 0$$
 Eq (6)

Integrating

$$\int \left(\frac{dp}{\rho} + gdz + \frac{1}{2}dV^2\right) = contt \qquad \text{Eq (7)}$$

 Assuming incompressible and steady flow

$$\frac{P}{\rho} + gz + \frac{1}{2}V^2 = contt \qquad \text{Eq (8)}$$

Dividing each equation by g

9
$$\frac{P}{\rho g} + z + \frac{V^2}{2g} = contt$$
 Eq (9)

 Hence Eq (9) for steadincompressible fluid assuming no frictional losses can be written as

$$Z_{1} + \frac{P_{1}}{\gamma} + \frac{V_{1}^{2}}{2g} = Z_{2} + \frac{P_{2}}{\gamma} + \frac{V_{2}^{2}}{2g}$$
(Total Head)₁ = (Total Head)₂ Eq (10)

Above Eq(10) is general form of Bernoulli's Equation

$$\frac{P}{\gamma} + z + \frac{V^2}{2g} = H$$

Pressure head + Elevation head + Velocity head = Total Head

Multiplying with unit weight, γ ,

$$P + \rho gz + \rho \frac{V^2}{2} = contt$$

- Static Pressure : P
- Dynamic pressure : $\rho V^2/2$
- Hydrostatic Pressure: $\rho g Z$
- Stagnation Pressure: Static pressure + dynamic Pressure $P + \rho \frac{V^2}{2} = P_{stag}$

Measurement of Heads

Piezometer: It measures pressure head (P/γ).

Pitot tube: It measures sum of pressure and velocity heads i.e.,

$$\frac{P}{\gamma} + \frac{V^2}{2g}$$



- Energy line: It is line joining the total heads along a pipe line.
- HGL: It is line joining pressure head along a pipe line.





13