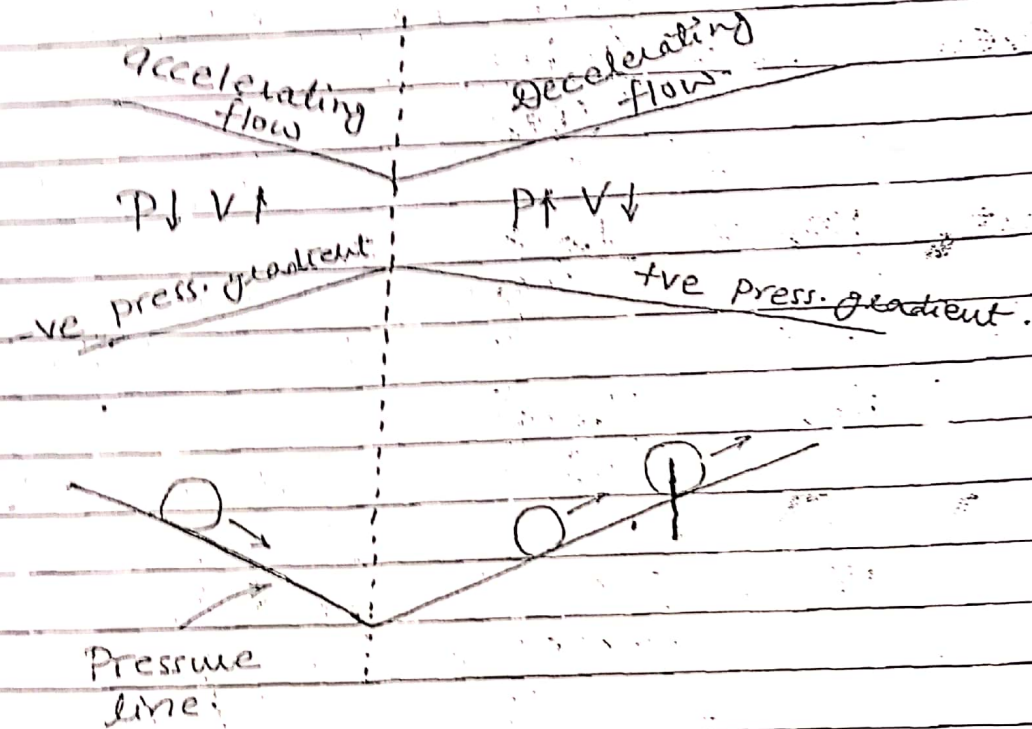


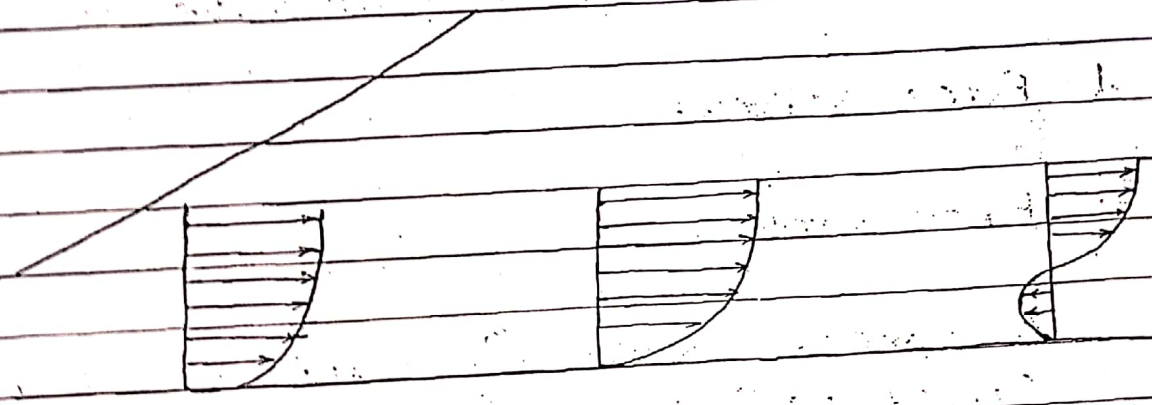
Boundary layer separation:



In case of convergent flow the velocity increases & pressure decreases & the fluid slides down the pressure line. When fluid flow in divergent passage the velocity decreases & pressure increases. i.e. The fluid moves under positive pressure gradient & hence it has to climb pressure hill. If the velocity reduction, its momentum of particle may not be support to climb a pressure hill & hence the flow may reverse its direction from boundary & this is known as boundary layer separation & reversal of flow & this occurs under +ve press. gradient's & These press. gradient is also known as

adverse press. gradient.

NOTE- For a fully developed flow the velocity profile remain's same.



$$\left. \frac{du}{dy} \right|_{y=0} = +ve$$

NO separation.
(Attached flow)

$$\left. \frac{du}{dy} \right|_{y=0} = 0$$

About to separate.
Separation point.
 $\tau = 0$

$$\left. \frac{du}{dy} \right|_{y=0} = -ve$$

separated flow.
detached flow

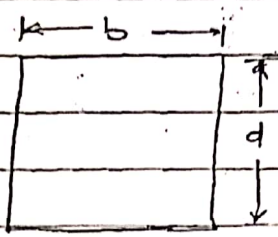
NOTE- The max. Thickness of boundary layer in pipe flow is equal to radius of pipe.

NOTE- Reynold's number in non-circular pipes.

$$Re = \frac{\rho V D_{eq}}{\mu}$$

where $D_{equivalent} = \frac{4A}{P}$ $A = \text{Area}$
 $P = \text{Perimeter}$

e.g. $D_{eq} = \frac{4(bd)}{2(b+d)}$



$$D_{eq} = \frac{2bd}{b+d}$$

Prob-105 For a velocity profile in laminar boundary layer -

$$\frac{u}{u_{\infty}} = \frac{3y}{2\delta} - \frac{y^3}{2\delta^3}$$

then find -

- (i) Boundary layer thickness.
- (ii) shear stress on the surface of the plate.
- (iii) Drag force.
- (iv) Average drag coefficient in terms of Reynold's number.

Soln:-

$$\tau_p = \rho u_{\infty}^2 \frac{d\theta}{dx}$$

$$T_o = \rho u_{\infty}^2 \frac{d\theta}{dx}$$

Momentum thickness,

$$\theta = \int_0^{\delta} \frac{u}{u_{\infty}} \left(1 - \frac{u}{u_{\infty}} \right) dy$$

$$\theta = \int_0^{\delta} \left(\frac{3y}{2\delta} - \frac{y^3}{2\delta^3} \right) \left\{ 1 - \left(\frac{3y}{2\delta} - \frac{y^3}{2\delta^3} \right) \right\} dy$$

$$\theta = \frac{39\delta}{280}$$

then $\tau_0 = \rho u_{\infty}^2 \times \frac{d}{dx} \left(\frac{39\delta}{280} \right)$

$$\tau_0 = \frac{39}{280} \cdot \rho u_{\infty}^2 \frac{d\delta}{dx} \quad \text{--- (1)}$$

we know that,

$$\tau = \mu \frac{du}{dy}$$

$$\frac{u}{u_{\infty}} = \frac{3y}{2\delta} - \frac{y^3}{2\delta^3}$$

$$u = u_{\infty} \left[\frac{3y}{2\delta} - \frac{y^3}{2\delta^3} \right]$$

$$\frac{du}{dy} = u_{\infty} \left[\frac{3}{2\delta} - \frac{3y^2}{2\delta^3} \right]$$

$$\frac{du}{dy} = u_{\infty} \left[\frac{3}{2s} - \frac{3y^2}{2s^2} \right]$$

$$\frac{du}{dy} \Big|_{y=0} = \frac{3u_{\infty}}{2s}$$

$$\tau_0 = \mu \frac{du}{dy} \Big|_{y=0}$$

$$\tau_0 = \mu \times \frac{3u_{\infty}}{2s}$$

$$\tau_0 = \frac{3\mu u_{\infty}}{2s} \quad \text{--- (11)}$$

from eqn. (1) & (11),

$$\frac{39}{280} \rho u_{\infty}^2 \frac{ds}{dx} = \frac{3\mu u_{\infty}}{2s}$$

$$\frac{13}{140} \rho u_{\infty} \frac{ds}{dx} = \frac{\mu}{s}$$

$$\frac{13}{140} \frac{\rho u_{\infty}}{\mu} s ds = dx$$

Integrate above eqn.

$$\frac{13}{140} \frac{\rho u_{\infty}}{\mu} \frac{s^2}{2} = x + C$$

At $x=0$, $\delta=0 \Rightarrow C=0$.

$$\frac{13}{280} \frac{\rho U_{\infty} \delta^2}{\mu} = x$$

multiplied by x in both side.

$$\frac{13}{280} \frac{\rho U_{\infty} x \delta^2}{\mu} = x^2$$

$$\frac{13}{280} x \text{Re}_x \cdot \delta^2 = x^2$$

$$\delta^2 = \frac{280 x^2}{13 \text{Re}_x}$$

$$\delta = \sqrt{\frac{280}{13}} \frac{x}{\sqrt{\text{Re}_x}}$$

$$\delta = \frac{4.64 x}{\sqrt{\text{Re}_x}}$$

$$\delta = \frac{4.64 x}{\sqrt{\frac{\rho U_{\infty} x}{\mu}}}$$

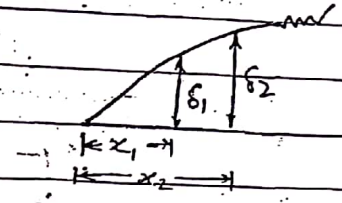
$$\delta \propto \frac{x}{\sqrt{x}}$$

$$\delta \propto x^{1/2}$$

δ vary with parabolically.

$$\delta \propto \sqrt{x}$$

δ_2	$=$	$\frac{\sqrt{x_2}}{\sqrt{x_1}}$
δ_1		



This is valid only for laminar boundary layer.

(ii) from eqn. (ii),

$$\tau_0 = \frac{3\mu U_\infty}{2\delta}$$

$$\tau_0 = \frac{3\mu U_\infty}{2 \times 4.64x \sqrt{Re_x}}$$

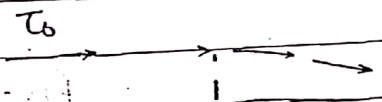
$$\tau_0 = \frac{3}{2 \times 4.64} \mu U_\infty \frac{\sqrt{Re_x}}{x}$$

$\tau_0 =$	$0.323 \mu U_\infty \frac{\sqrt{Re_x}}{x}$
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$$\tau_0 \propto \frac{1}{x}$$

$$\tau_0 \propto \frac{1}{x^{1/2}}$$

$$\tau_0 \propto x^{-1/2}$$

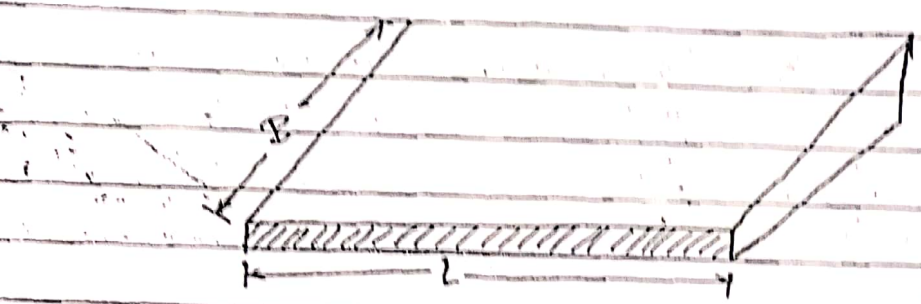


shear stresses decreases along length.

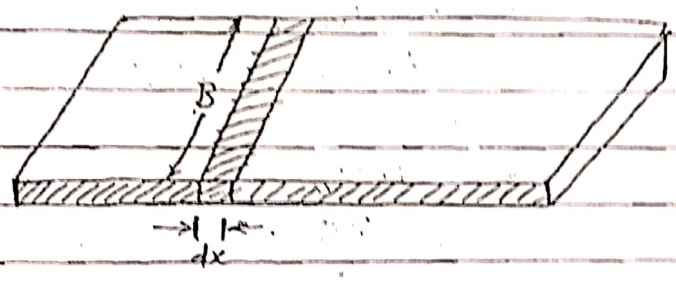
τ_{01}	$=$	$\frac{\sqrt{x_2}}{\sqrt{x_1}}$
τ_{02}		

Shear stress vary with inversely proportional.

(iii)



As the shear stress T_0 vary with length then take small element and find the drag force in small element & then integrate for finding total drag force.



The drag force on small element.

$$dF_D = T_0 \times B dx$$

Total drag force.

$$F_D = \int_0^L T_0 \times B dx$$

$$F_D = \int_0^L 0.323 \frac{\mu U_\infty \sqrt{Re_x}}{x} B dx$$

$$F_D = \int_0^L 0.323 \frac{\mu U_\infty}{x} \sqrt{\frac{\rho U_\infty x}{\mu}} B dx$$

$$F_D = 0.323 \mu U_\infty B \frac{\sqrt{\rho U_\infty}}{\sqrt{\mu}} \int_0^L \frac{1}{\sqrt{x}} dx$$

$$F_D = 0.323 \mu U_{\infty} B \frac{\sqrt{\rho U_{\infty}}}{\sqrt{\mu}} [2\sqrt{L}]$$

$$F_D = 0.646 \mu U_{\infty} B \cdot \sqrt{\rho} \sqrt{U_{\infty}} \sqrt{L}$$

$$F_D = 0.646 \mu U_{\infty} B \sqrt{\frac{\rho U_{\infty} L}{\mu}}$$

$$F_D = 0.646 \mu U_{\infty} B \cdot \sqrt{Re_L}$$

$$C_D = \frac{F_D}{\frac{1}{2} \rho A U_{\infty}^2}$$

$$C_D = \frac{0.646 \mu U_{\infty} B \sqrt{Re_L}}{\frac{1}{2} \rho A U_{\infty}^2}$$

$$C_D = \frac{1.292 \mu \sqrt{Re_L}}{\rho L U_{\infty}}$$

$$C_D = \frac{1.292 \sqrt{Re_L}}{\rho U_{\infty} L}$$

$$C_D = \frac{1.292 \sqrt{Re_L}}{Re_L}$$

$C_D = \frac{1.292}{\sqrt{Re_L}}$

∴ When velocity profile is not given use the following eqn. (Blausius equation)

Laminar	Turbulent
$\delta = 5x$ $\sqrt{Re_x}$	$\delta = 0.576x$ $(Re)^{1/2}$
$C_{fx} = 0.664$ $\sqrt{Re_x}$	$C_{fx} = 0.059$ $(Re)^{1/2}$
$C_D = 1.328$ $\sqrt{Re_L}$	$C_D = 0.074$ $(Re)^{1/2}$

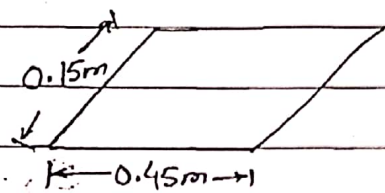
Prob-106 - Calculate the drag force on the plate 0.15m wide & 0.45m long placed in a stream of oil having a free stream velocity of 6m/s. also find the thickness of boundary layer & shear stress at the trailing edge. The density of oil has 925 kg/m^3 & kinematic viscosity is equal to $0.9 \times 10^{-4} \text{ m}^2/\text{s}$.

Solⁿ:

$$Re_L = \frac{\rho U_{\infty} L}{\mu}$$

$$Re_L = \frac{U_{\infty} L}{\nu} = \frac{U_{\infty} L}{\frac{\mu}{\rho}}$$

$$Re_L = \frac{6 \times 0.45}{0.9 \times 10^{-4}} = 3 \times 10^4$$



As $Re_L < 10^5$
flow in the boundary layer is laminar.

(i)
$$C_D = \frac{F_D}{\frac{1}{2} \rho A U_{\infty}^2} = \frac{1.328}{\sqrt{Re_L}}$$

$$\frac{F_D}{\frac{1}{2} \times 925 \times 0.15 \times 0.45 \times 6^2} = \frac{1.328}{\sqrt{3 \times 10^4}}$$

$$F_D = 8.6 \text{ N} \quad \text{Ans.}$$

This is the drag force on one side of the plate.

(ii) Shear stress at the trailing edge.

$$C_{fx} = \frac{0.664}{\sqrt{Re_x}} = \frac{\tau_0}{\frac{1}{2} \rho U_{\infty}^2}$$

$$= \frac{0.664}{\sqrt{3 \times 10^4}} = \frac{\tau_0}{\frac{1}{2} \times 925 \times 6^2}$$

$$\tau_0 = 63.8 \text{ N/m}^2 \quad \text{Ans.}$$

(iii) Boundary layer thickness.

$$\delta = \frac{5x}{\sqrt{Re_x}} = \frac{5 \times 0.45}{\sqrt{3 \times 10^4}}$$

$$\delta = 0.0129 \text{ m} \quad \text{Ans.}$$

prob-107 - For an air flow over a flat plate the velocity u & boundary layer thickness δ can be expressed as -

$$u = \frac{3y}{2\delta} \frac{y^3}{2\delta^3}$$

& $\delta = \frac{4.64x}{\sqrt{Re_x}}$ If $U_{\infty} = 2 \text{ m/s}$.

$\mu_{\text{air}} = 1.5 \times 10^{-5} \text{ m}^2/\text{sec}$.

$\rho = 1.32 \text{ kg/m}^3$.

find the shear stress on the surface of plate at $x = 1 \text{ m}$.

Solⁿ: given,

$$u = \frac{3y}{2\delta} \frac{y^3}{2\delta^3}$$

$$u = U_{\infty} \left[\frac{3y}{2\delta} \frac{y^3}{2\delta^3} \right]$$

$$\frac{du}{dy} = U_{\infty} \left[\frac{3(1) - 3y^2}{2\delta} \frac{1}{2\delta^3} \right]$$

$$\left. \frac{du}{dy} \right|_{y=0} = U_{\infty} \left[\frac{3}{2\delta} \right]$$

& $\tau_0 = \mu \left. \frac{du}{dy} \right|_{y=0}$

$$\tau_0 = \mu \times \frac{3U_{\infty}}{2\delta} \quad \text{--- (1)}$$

given $\delta = \frac{4.64x}{\sqrt{Re_x}}$

but $Re_x = \frac{U_{\infty} \cdot x}{\mu/\rho}$

$$Re_x = \frac{U_{\infty} \cdot x}{\nu}$$

$$Re_x = \frac{2 \times 1}{1.5 \times 10^{-5}} = 1.33 \times 10^5$$

then $\delta = \frac{4.64 \times 1}{\sqrt{1.33 \times 10^5}} = 0.0127 \text{ m.}$

Now put the value in eqn. (1):

$$\tau_0 = \frac{3 \times 1.5 \times 10^{-5} \times 1.23 \times 2}{2 \times 0.0127}$$

$$\tau_0 = 4.35 \times 10^{-3} \text{ N/m}^2 \text{ (Ans.)}$$