

Reciprocating compressor

1. A single stage reciprocating compressor takes 1 m^3 of air per minute at 1.013 bar and 15°C and delivers it at 7 bar. Assuming that the law of compression is $P_v^{1.35} = \text{constant}$, and the clearance is negligible, calculate the indicated power?

Solution

Volume of air taken in, $V_1 = 1\text{ m}^3/\text{min}$

Intake pressure, $p_1 = 1.013\text{ bar}$

Initial temperature, $T_1 = 15 + 273 = 288\text{ K}$

Delivery pressure, $P_2 = 7\text{ bar}$

Law of compression: $P_v^{1.35} = \text{constant}$

Indicated power I.P.:

Mass of air delivered per min.,

$$m = \frac{p_1 v_1}{RT_1} = \frac{1.013 \times 10^5 \times 1}{287 \times 288} = 1.266\text{ kg / min}$$

$$\begin{aligned} \text{Delivery temperature, } T_2 &= T_1 \left(\frac{p_2}{p_1} \right)^{(n-1/n)} \\ &= 288 \left(\frac{7}{1.013} \right)^{(1.35-1)/1.35} = 475.2\text{ K} \end{aligned}$$

$$\begin{aligned} \text{Indicated work} &= \frac{n}{n-1} mR(T_2 - T_1)\text{ kJ / min} \\ &= \frac{1.35}{1.35-1} \times 1.226 \times 0.287(475.2 - 288) = 254\text{ kJ / min} \end{aligned}$$

$$\text{i.e., Indicated power I.P} = \frac{254}{60} = 4.23\text{ kW. (Ans)}$$

2. An air compressor cylinder has 150mm bore and 150mm stroke and the clearance is 15%. It operates between 1 bar, 27°C and 5 bar. Take polytropic exponent $n=1.3$ for compression and expansion processes find?

- i. Cylinder volume at the various salient points of in cycle.
- ii. Flow rate in m^3/min at 720 rpm and .
- iii. The deal volumetric efficiency.

Given

$$D = 150 \times 10^{-3} \text{ m} \quad P_2 = 5 \times 10^5 \text{ N/m}^2$$

$$L = 150 \times 10^{-3} \text{ m} \quad T_1 = 27 + 273 = 300 \text{ K}$$

$$V_c = 0.15 V_s \quad N = 720 \text{ rpm}$$

$$P_1 = 1 \times 10^5 \text{ N/m}^2 \quad p v^n = C n = 1.3$$

Find

- i. V_1, V_2, V_3, V_4
- ii. FAD (V_a)
- iii. η_v

Solution

$$V_1 = V_c + V_s$$

$$V_s = \frac{\pi}{4} D^2 L N = \frac{\pi}{4} (0.15)^2 \times 0.15 \times 720 = 1.9085 \text{ m}^3 / \text{min}$$

$$V_c = 0.15 V_s$$

$$= 0.15 \times 1.9085$$

$$V_c = 0.2862 \text{ m}^3 / \text{min}$$

$$V_1 = V_c + V_s$$

$$= 0.2862 + 1.9085$$

$$\boxed{V_1 = 2.1948} \text{ m}^3 / \text{min}$$

$$P_1 V_1^n = P_2 V_2^n$$

$$V_2 = V_1 \left(\frac{P_1}{P_2} \right)^{1/n}$$

$$= 2.1948 \left(\frac{1 \times 10^5}{5 \times 10^5} \right)^{1/1.3}$$

$$V_2 = 0.6366 \text{ m}^3/\text{min}$$

$$V_3 = 0.2862 \text{ m}^3/\text{min} = V_c$$

$$V_c = V_3 \quad \therefore$$

$$P_3 V_3^n = P_4 V_4^n$$

$$V_4 = V_3 \left(\frac{P_3}{P_4} \right)^{1/n}$$

WKT

$$P_2 = P_3$$

$$P_1 = P_4$$

$$\therefore V_4 = V_3 \left(\frac{P_2}{P_1} \right)^{1/n}$$

$$= 0.2862 \left[\frac{5 \times 10^5}{1 \times 10^5} \right]^{1/1.3}$$

$$V_4 = 0.98674 \text{ m}^3/\text{min}$$

$$\therefore \text{Volumetric efficiency } (\eta_v) = 1 + k - k \left(\frac{P_2}{P_1} \right)^{1/n}$$

$$k = \text{Clearance Ratio} = \frac{V_c}{V_s} = \frac{0.2862}{1.9085}$$

$$K = 0.1499$$

$$\therefore \eta_v = 1 + 0.1499 - 0.1499 \left[\frac{5}{1} \right]^{1/1.3}$$

$$\eta_v = 0.633 = 63.3\%$$

$$\eta_v = 63.3\%$$

∴ WKT

$$\eta_v = \frac{FAD}{V_s}$$

$$\begin{aligned}\therefore FAD &= \eta_v \times V_s \\ &= 0.633 \times 1.9085\end{aligned}$$

$$FAD = 1.2083 \text{ m}^3/\text{min}$$

3. Calculate the diameter and stroke for a double acting single stage reciprocating air compressor of 50kW having induction pressure 100 kN/m^2 and temperature 150°C . The law of compression is $PV^{1.2} = C$ and delivery pressure is 500 kN/m^2 . The revolution/sec = 1.5 and mean piston speed is 150 m/min. Clearance is neglected.

Given:

Double acting single stage

Compressor

IP = 50kW

$P_1 = 100 \times 10^3 \text{ N/m}^2$

$T_1 = 15 + 273 = 288\text{K}$

$PV^{1.2} = C \quad \therefore n=1.2$

$P_2 = 500 \times 10^3 \text{ N/m}^2$

$N = 1.5 \text{ rps} = 1.5 \times 60 \text{ rpm}$

$2LN = 150 \text{ m/min}$ (Double acting)

Find

i. D and L

Solution

For double acting compressor average piston speed = $2LN$

∴ $2LN = 150 \text{ m/min}$

$$\therefore L = \frac{150}{2 \times 1.5 \times 60} = 0.833 \text{ m}$$

$$L = 0.833 \text{ m}$$

To Find D

$$IP = W.N_w$$

where

N_w = Number of working stroke

For Double acting $N_w = 2N$

For single acting $N_w = N$

$$\therefore N_w = 2 \times 1.5 \times 60 = 180 \text{ rpm}$$

$$\therefore W.D/\text{cycle} = \frac{n}{n-1} p_1 V_1 \left[\left(\frac{p_2}{p_1} \right)^{\frac{n-1}{n}} - 1 \right]$$

$$= \frac{1.2}{1.2-1} \times 100 \times 10^3 \left(\frac{\pi}{4} D^2 \times 0.833 \right) \times \left[\left(\frac{500}{100} \right)^{\frac{0.2}{1.2}} - 1 \right]$$

$$W = 120764.2 D^2$$

N-m

$$\therefore IP = \frac{W.N_w}{60}$$

$$50 \times 10^3 = \frac{120764.2 D^2 \times 180}{60}$$

$$D^2 = 0.1380$$

$$D = 0.371 \text{ m}$$

4. A single acting reciprocating air compressor has cylinder diameter and stroke of 200 mm and 300 mm respectively. The compressor sucks air at 1 bar and 27°C and delivers at 8 bar while running at 100 r.p.m Find: 1. Indicated power of the compressor; 2. Mass of air delivered by the compressor per minute; and 3. temperature of the delivered by the compressor. The compression follows the law $PV^{1.25} = C$ Take R as 287 J/kg K.

Solution.

Given

$$D = 200 \text{ mm} = 0.2 \text{ m};$$

$$L = 300 \text{ mm} = 0.3 \text{ m};$$

$$p_1 = 1 \text{ bar} = 1 \times 10^5 \text{ N/m}^2$$

$$T_1 = 27^\circ\text{C} = 27 + 273 = 300\text{K};$$

$$p_2 = 8 \text{ bar};$$

$$N = 100 \text{ r.p.m}$$

$$n=1.25;$$

$$R= 287 \text{ J/kg K}$$

1. Indicated power of the compressor

$$V_1 = \frac{\pi}{4} D^2 L = 0.0094 \text{ m}^3$$

We know that workdone by the compressor for polytropic compression of air as

$$\begin{aligned} W &= \frac{n}{n-1} p_1 V_1 \left[\left(\frac{p_2}{p_1} \right)^{\frac{n-1}{n}} - 1 \right] \\ &= \frac{1.25}{1.25-1} \times 1 \times 10^5 \times 0.0094 \left[\left(\frac{8}{1} \right)^{\frac{1.25}{1.25-1}} - 1 \right] \text{ N-m} \\ &= 4700(1.516-1) = 2425 \text{ N-m} \end{aligned}$$

Since the compressor is single acting, therefore number of working strokes per minute,

$$N_w = N = 100$$

∴ Indicated power of the compressor

$$= \frac{W \times N_w}{60} = \frac{2425 \times 100}{60} = \mathbf{4042 \text{ kW}}$$

2. Mass of air delivered by the compressor per minute

Let m = Mass of air delivered by the compressor per stroke.

$$\text{We know that } P_1 V_1 = mRT_1$$

$$\therefore m = \frac{P_1 V_1}{RT_1} = \frac{1 \times 10^5 \times 0.0094}{287 \times 300} = 0.0109 \text{ kg per stroke}$$

$$\text{and mass delivered minute} = m \times N_w = 0.0109 \times 100 = \mathbf{1.09 \text{ kg}}$$

3. Temperature of air delivery by the compressor

Let T_2 = Temperature of air delivered by the compressor.

We know that
$$\frac{T_2}{T_1} = \left(\frac{p_2}{p_1}\right)^{\frac{n-1}{n}} = \left(\frac{8}{1}\right)^{\frac{1.25-1}{1.25}} = 8^{0.2} = 1.516$$

$$T_2 = 1.516 \times T_1 = 1.516 \times 300 = 454.8 \text{ K} = 181.8^\circ \text{K}$$

5. A single –stage double –acting air compressor is required to deliver 14 m³ of air per minute measured at 1.013 bar and 150°C. The delivery pressure is 7 bar and the speed 300 r.p.m. Take the clearance volume as 5% of the swept volume with the compression and expansion index of $\eta = 1.3$ Calculate:

- i. Swept volume of the cylinder;
- ii. The delivery temperature;
- iii. Indicated power.

Solution

Quantity of air to be delivered	=	14 m ³ /min
Intake pressure and temperature	p_1	= 1.013 bar,
	T_1	= 15 + 273 = 288 K
Delivery pressure	p_2	= 7 bar
Compressor speed,	N	= 300 r.p.m
Clearance volume,	V_c	= 0.05 V_s
Compression and expansion index	n	= 1.3

Swept volume of the cylinder, V_s :

$$\text{Swept volume } V_s = V_1 - V_3 = V_1 - V_c = V_1 - 0.05 V_s$$

$$V_1 - V_4 = \frac{\text{FAD}}{N_w}$$

$$\text{and } V_1 - V_4 = \frac{14}{300 \times 2} = 0.0233 \text{ m}^3$$

$$\text{Now, } V_1 = 1.05 V_s \text{ and } \frac{V_4}{V_3} = \left(\frac{p_2}{p_1}\right)^{\frac{1}{n}} = \left(\frac{7}{1.013}\right)^{\frac{1}{1.3}} = 4.423$$

$$\text{i.e., } V_1 - V_3 = 4.423 V_3 = 4.423 \times 0.05 V_s = 0.221 V_s$$

$$\therefore (V_1 - V_4) = 1.05 V_s - 0.221 V_s = 0.829 V_s = 0.0233 \text{ m}^3$$

$$\therefore V_8 \frac{0.0233}{1.05 - 0.221} = 0.0281 \text{ m}^3$$

i.e Swept volume of the cylinder = 0.0281 m³ .

ii. The delivery temperature, T₂

Using the relation
$$\frac{T_2}{T_1} = \left(\frac{p_2}{p_1} \right)^{\frac{n-1}{n}}$$

$$\therefore T_2 = T_1 \times \left(\frac{p_2}{p_1} \right)^{\frac{n-1}{n}} = 288 \times \left(\frac{7}{1.013} \right)^{\frac{1.3-1}{1.3}} = 450 \text{ K}$$

$$\therefore \text{Delivery temperature} = 450 - 273 = 177^\circ\text{C}$$

iii Indicated power:

$$\begin{aligned} \text{Indicated power} &= \frac{n}{n-1} p_1 (V_1 - V_4) \left\{ \left(\frac{p_2}{p_1} \right)^{\frac{n-1}{n}} - 1 \right\} \\ &= \frac{1.3}{1.3-1} \times \frac{1.013 \times 10^5 \times 14}{10^3 \times 6} \left\{ \left(\frac{7}{1.013} \right)^{\frac{1.3-1}{1.3}} - 1 \right\} \\ &= 57.56 \text{ kW} \end{aligned}$$

$$\text{Indicated power} = 57.56 \text{ kW}$$

6. A single stage single acting air compressor delivers 0.6 kg of air per minute at 6 bar . The temperature and pressure at the end of suction stroke are 30°C and 1 bar. The bore and stroke of the compressor are 100 mm and 150 mm respectively. The clearance is 3% of the swept volume Assuming the index of compression and expansion to be 1.3. find:

- i. Volumetric efficiency of the compressor
- ii. Power required if the mechanical efficiency is 85%, and
- iii. Speed of the compressor (r.p.m)

Given

Mass of air delivered,	m=0.6kg/min
Delivery Pressure,	p ₂ =6 bar
Induction Pressure,	p ₁ =6 bar

Induction temperature, $T_1 = 30 + 273 = 303 \text{ K}$
 Bore, $D = 100\text{mm} = 0.1 \text{ m}$
 Stroke length, $L = 150\text{mm} = 0.15 \text{ m}$
 Clearance volume, $V_c = 0.03 V_s$
 Mechanical efficiency $\eta_{\text{mech}} = 85\%$

i. Volumetric efficiency of the compressor, η_{vol} :

$$\eta_{\text{vol}} = 1 + k - k \left(\frac{P_2}{P_1} \right)^{\frac{1}{n}}$$

Where $k = \frac{V_c}{V_s} = 0.03$

$$\therefore \eta_{\text{vol}} = 1 + 0.03 - 0.03 \left(\frac{6}{1} \right)^{\frac{1}{1.3}} = 0.91096 \text{ or } 91.096\%$$

ii. Power required if the mechanical efficiency is 85%, and

$$\text{Indicated power} = \frac{n}{n-1} mRT_1 \left[\left(\frac{P_2}{P_1} \right)^{\frac{n-1}{n}} - 1 \right]$$

$$\frac{1.3}{1.3-1} \times \frac{0.6}{60} \times 0.287 \times 303 \left[\left(\frac{6}{1} \right)^{\frac{1.3-1}{1.3}} - 1 \right] = 1.93 \text{ kW}$$

$$\therefore \text{Power required to drive the compressor} = \frac{1.93}{\eta_{\text{mech}}} = \frac{1.93}{0.85} = 2.27 \text{ kW}$$

iii. Speed of the compressor (r.p.m)

$$\text{Free air delivery, F.A.D} = \frac{mRT_1}{P_1} \times \frac{0.6 \times 0.287 \times 1000 \times 303}{1 \times 10^5} = 0.5218 \text{ m}^3/\text{min}$$

$$\text{Displacement volume} = \frac{\text{F.A.D}}{\eta_{\text{vol}}} = \frac{0.5218}{0.91096} = 0.5728 \text{ m}^3/\text{min}$$

Also $0.5728 = \frac{\pi}{4} D^2 L \times N$ (for single – acting compressor)

or $0.5728 = \frac{\pi}{4} 0.1^2 \times 0.15 \times N$

$$\therefore \text{Speed of compressor } N = \frac{0.5728 \times 4}{\pi \times 0.1^2 \times 0.15} = 486.2 \text{ r.p.m}$$

7.A single stage , single air compressor running at 1000 r.p.m delivers air at 25 bar . For this purpose the induction and free air conditions can be taken as 1.013 bar and 15°C and the free air delivery as 0.25 m³/min. The clearance volume is 3% of the swept volume and the stroke bore ratio is 1:2:1 Take the index of compression and expansion as 1.3. calculate also the indicated power and the isothermal efficiency

Given data:-

With clearance volume

Single stage single acting air compressor

N=1000 rpm

$p_2 = 25 \text{ bar} = 25 \times 10^5 \text{ N/m}^2$

$T_1 = 15^\circ = 273 + 15 = 288 \text{ K}$

$V_c = 0.03 V_s$

$$\frac{V_c}{V_s} = k = 0.03$$

$$\frac{\text{Stroke}(D)}{\text{Bore}(L)} = \frac{1}{2}$$

$$L = 2D$$

$$n = 1.3$$

$PV^n = C$ (polytropic process) To find

i. η_v , D and L

ii. (I.P) and η_{Iso}

$$\text{i. } \eta_v = 1 + k - k \left(\frac{P_2}{P_1} \right)^{\frac{1}{n}}$$

$$\eta_v = 1 + 0.03 - 0.03 \left(\frac{25 \times 10^5}{1.013 \times 10^5} \right)^{\frac{1}{1.3}}$$

$$\eta_v = 0.6766$$

$$\text{ii. } IP = \frac{W_{poly} \times N}{60}$$

Inductor power = I.P

$$W_{poly} = \frac{n}{n-1} p(V_1 - V_4) \left[\left(\frac{P_2}{P_1} \right)^{\frac{n-1}{n}} \right]$$

$$\therefore \eta_v = \frac{FAD/V_a}{V_s}$$

$$V_s = \frac{V_a}{\eta_v} = \frac{0.25}{0.6766}$$

$$V_s = 0.369 \text{ m}^3/\text{min}$$

$$V_s = \frac{\pi}{4} \times D^2 \times L$$

$$0.369 = \frac{\pi}{4} \times D^2 \times 2D = \frac{\pi D^3}{2}$$

$$D = 0.617 \text{ m} = 617 \text{ mm}$$

$$L = 2D = 2 \times 0.617$$

$$L = 1234 \text{ mm}$$

$$V_c = 0.011 \text{ m}^3/\text{min} = V_3$$

$$V_1 = V_c + V_s$$

$$V_1 = 0.011 + 0.369$$

3-4 is expansion

$$pv^n = C$$

$$\frac{P_4}{P_3} = \left(\frac{v_3}{v_4} \right)^n$$

$$\frac{v_4}{v_3} = \left(\frac{P_3}{P_4} \right)^{\frac{1}{n}} = \left(\frac{P_2}{P_1} \right)^{\frac{1}{n}}$$

$$V_4 = V_3 \left(\frac{P_2}{P_1} \right)^{\frac{1}{n}}$$

$$V_4 = 0.129 \text{ m}^3/\text{min}$$

$$W_{poly} = \left(\frac{n}{n-1} \right) p (V_1 - V_4) \left[\left(\frac{P_2}{P_1} \right)^{\frac{n-1}{n}} \right]$$

$$= \frac{1.3}{0.3} \times 1.013 \times 10^5 (0.38 - 0.129) \left[\left(\frac{2.5}{1.013} \right)^{\frac{0.3}{1.3}} - 1 \right]$$

$$W.D_{poly} = 120713.193 \text{ N}\cdot\text{min}$$

$$I.P = \frac{W.D_{poly} \times N}{60}$$

$$I.P = \frac{12713 \times 1000}{60}$$

$$\eta_{iso} = \frac{W_{iso}}{W_{poly}}$$

$$W_{iso} = p_1 (V_1 - V_2) \ln \left(\frac{P_2}{P_1} \right)$$

$$\eta_{iso} = \frac{p_1 (V_1 - V_2) \ln \left(\frac{P_2}{P_1} \right)}{\left(\frac{n}{n-1} \right) p_1 (V_1 - V_4) \left[\left(\frac{P_2}{P_1} \right)^{\frac{n-1}{n}} - 1 \right]}$$

$$\eta_{iso} = \frac{1.013 \times 10^5 \times (0.0380 - 0.129) \ln \left(\frac{25}{1.013} \right)}{120713.19}$$

$$\eta_{iso} = 0.675$$

$$\eta_{iso} = 67.5\%$$

8. A two stage air compressor air from 1 bar and 20°C to 42 bar. If the law of compression is $p_v^{1.35} = \text{constant}$ and the intercooling is complete to 20°C, find per kg of air: 1. The work done is compressing; and 2. The mass of water necessary for abstracting the heat in the intercooler, if the temperature rise of the cooling water is 25°C

$$p_1 = 1 \text{ bar} = 1 \times 10^5 \text{ N/m}^2$$

$$T_1 = 20^\circ \text{C} = 20 + 273 = 293 \text{K}$$

$$p_3 = 42 \text{ bar} = 42 \times 10^5 \text{ N/m}^2$$

$$n = 1.35$$

$$T_3 = 20^\circ \text{C} = 20 + 273 = 293 \text{K}; m = 1 \text{ kg};$$

$$\text{Rise in temperature of cooling water} = 25^\circ \text{C};$$

$$R = 287 \text{ J/kg K } c_p = 1 \text{ kJ /kg K}$$

we know that for complete intercooling. the intercooler pressure

$$p_2 = \sqrt{p_1 p_3} = \sqrt{1 \times 42} = 6.48 \text{ bar}$$

and volume of air admitted for compression

$$V_1 \frac{mRT_1}{p_1} = \frac{1 \times 287 \times 293}{1 \times 10^5} = 0.84 \text{ m}^3 / \text{kg of air}$$

1. Work done compressing the air

$$W = \left(\frac{n}{n-1} \right) \times p_1 V_1 \left[\left(\frac{P_2}{P_1} \right)^{\frac{n-1}{n}} + \left(\frac{P_2}{P_1} \right)^{\frac{n-1}{n}} - 2 \right]$$

$$= \frac{1.35}{1.35-1} \times 1 \times 10^5 \times 0.84 \left[\left(\frac{6.48}{1} \right)^{\frac{1.35-1}{1.35}} + \left(\frac{42}{6.48} \right)^{\frac{1.35-1}{1.35}} - 2 \right] \text{ N-m}$$

$$= 3.24 \times 10^5 (1.62 + 1.62 - 2) = 4.017 \times 10^5 \text{ N-m}$$

2. Mass of water necessary for abstracting the heat in the intercooler.

Let $m_w =$ Mass of water necessary /kg of air ,and

$T_2 =$ Temperature of the air entering the intercooler.

$$\frac{T_2}{T_1} = \left(\frac{P_2}{P_1} \right)^{\frac{n-1}{n}} = \left(\frac{6.48}{1} \right)^{\frac{1.35-1}{1.35}} = 1.622$$

$$T_2 = T_1 \times 1.622 = 293 \times 1.622 = 475.6 \text{ K}$$

We know that heat gained by water

$$= \text{Heat lost by air}$$

$$\therefore m_w \times c_w \times \text{Rise in temperature}$$

$$= m c_p (T_2 - T_3)$$

$$m_w \times 4.2 \times 25 = 1 \times 1 (475.6 - 293) = 182.6$$

$$m_w = 1.74 \text{ kg}$$

9.A two- stage acting reciprocating compressor takes in air at the rate of 0.2 m³/s. The intake pressure and temperature of air 0.1MP_a and 16°C. The air is compressed to a final pressure of .7MP_a. The intermediate pressure is ideal and intercooling is perfect. The compression index in both the stages is 1.25 and the compressor runs at 600 r.p.m. Neglecting clearance determine:

- i. The intermediate pressure
- ii. The total volume of each cylinder,
- iii. The power required to drive the compressor and
- iv. The rate of heat rejection in the intercooler.

Take $c_p = 1.005 \text{ kJ/kg K}$ and $R = 0.287 \text{ kJ/kg K}$

Solution .

Intake volume $V_1 = 0.2 \text{ m}^3/\text{s}$

Intake pressure $p_1 = 0.1 \text{ MP}_a$

Intake temperature $T_1 = 16 + 273 = 289 \text{ K}$

Final pressure $p_3 = 0.7 \text{ MP}_a$

Compression index in both stages, $n_1 = n_2 \quad n = 1.25$

Speed of the compressor $N = 600 \text{ r.p.m}$

$$c_p = 1.005 \text{ kJ/kg K}; R = 0.287 \text{ kJ/kg K}$$

- i. The power required to drive the compressor, P_2 :**

$$p_2 = \sqrt{p_1 p_3} = \sqrt{0.1 \times 0.7} = 0.2646 \text{ MP}_a$$

- ii. The total volume of each cylinder, V_{s1}, V_{s2} :**

$$\text{We know that } V_{s1} \times \frac{N}{60} = V_1 \text{ or } V_{s1} \times \frac{600}{60} = 0.2$$

$$\therefore V_{s1} \text{ (Volume of L.P cylinder)} = \frac{600 \times 0.2}{60} = 0.02 m^3 \text{ (Ans).}$$

$$\text{Also } p_1 V_{s1} = p_1 V_{s2} \text{ or } V_{s2} = \frac{p_1 V_{s1}}{p_2}$$

$$V_{s2} \text{ (Volume of H.P. Cylinder)} = \frac{0.1 \times 0.02}{0.2646} = 0.00756 m^3 \text{ (Ans)}$$

iii. The rate of heat rejection in the intercooler:

$$\text{Mass of air handled, } m = \frac{p_1 V_1}{RT_1} = \frac{(0.1 \times 10^3) \times 0.2}{0.287 \times 289} = 0.241 \text{ kg/s}$$

$$\text{Also, } \frac{T_2}{T_1} = \left(\frac{p_2}{p_1} \right)^{\frac{n-1}{n}} \text{ or } \frac{T_2}{289} = \left(\frac{0.2646}{0.1} \right)^{\frac{1.25-1}{1.25}} \text{ or } T_2 = 351.1 \text{ K}$$

$$\begin{aligned} \therefore \text{Heat rejected in the intercooler} &= m \times c_p \times (T_2 - T_1) \\ &= 0.241 \times 1.005 \times (351.1 - 289) = 15.04 \text{ kJ/s or } 15.04 \text{ kW. (Ans)} \end{aligned}$$

10. A single acting reciprocating air compressor has a swept volume of 2000 cm³ and runs at 800 rpm. It operates with pressure ratio of 8 and clearance of 5% of the swept volume. Inlet pressure and temperature are 1.013 bar, and 15°C respectively. Assume n=1.25 for both compression and expansion. Find

- i. Indicated power**
- ii. Volumetric efficiency**
- iii. Mass flow rate**
- iv. FAD**
- v. Isothermal efficiency**
- vi. Actual Power required to drive the compressor if $\eta_{\text{mech}}=85\%$**

Given

Single acting reciprocating compressor

$$V_s = 2000 \text{ cm}^3 = 0.002 \text{ m}^3$$

$$N = 800 \text{ rpm}$$

$$\frac{P_2}{P_1} = \frac{P_3}{P_4} = 8$$

$$\begin{aligned}
V_c &= 5\% V_s \\
&= 0.05 \times 0.002 \\
V_c &= 0.0001 \text{ m}^3 \\
p_1 &= 1.013 \times 10^5 \text{ N/m}^2 \\
T_1 &= 15 + 273 = 288 \text{ K} \\
P_V^n &= C \quad n = 1.25
\end{aligned}$$

Find: i) IP ii) η_v iii) m iv) FAD (V_a) v) η_{iso} vi) P_{act} if $\eta_m = 85\%$

Solution

WKT

$$\text{Clearance ratio (k)} = \frac{V_c}{V_s} = \frac{0.0001}{0.002}$$

k	=	0.05
---	---	------

$$\begin{aligned}
\therefore \text{Volumetric efficiency } (\eta_v) &= 1 + k - k \left(\frac{P_2}{P_1} \right)^{\frac{1}{n}} \\
&= 1 + 0.05 - 0.05 (8)^{1/1.25} \\
\eta_v &= 78.61\%
\end{aligned}$$

WKT

$$\begin{aligned}
\eta_v &= \frac{FAD}{V_s} \\
FAD &= \eta_v \times V_s \\
&= 0.7861 \times 0.002 \\
&= 1.5722 \times 10^{-3} \text{ m}^3
\end{aligned}$$

$$\begin{aligned}
\frac{FAD}{\text{min}} &= \frac{FAD}{\text{Stroke}} \times \text{Speed} \\
&= 1.5722 \times 10^{-3} \times 800
\end{aligned}$$

$$\therefore FAD = 1.2578 \text{ m}^3/\text{min}$$

To find mass flow rate

$$Pv = mRT$$

$$m = \frac{pV}{RT} = \frac{1.013 \times 10^5 \times 1.2578}{287 \times 288}$$

$$m = 1.542 \text{ kg/min}$$

To find – Indicated power

$$IP = \frac{W.D \times N_w}{\text{sec}}$$

$$N_w = N \text{ (single acting)} = 800 \text{ rpm.}$$

$$W.D = \frac{n}{n-1} mR(T_2 - T_1) \text{ kJ/min.}$$

$$T_2 = T_1 \left(\frac{P_2}{P_1} \right)^{\frac{n-1}{n}}$$

$$= 288(8)^{\frac{1.25-1}{1.25}}$$

$$T_2 = 436.53 \text{ K}$$

$$\therefore W.D = \frac{1.25}{0.25} \times 1.542 \times 0.287(436.53 - 288)$$

$$W.D = 328.66 \text{ kJ/min}$$

$$\therefore IP = \frac{W.D}{s} = \frac{328.66}{60}$$

$$IP = 5.48 \text{ kW}$$

To find isothermal efficiency

$$W_{iso} = P_1 V_1 \ln \left(\frac{P_2}{P_1} \right)$$

$$= mRT_1 \ln \left(\frac{P_2}{P_1} \right)$$

$$= 1.542 \times 0.287 \times 288 \times \ln(8)$$

$$(W.D)_{iso} = 265.04 \text{ kJ/min}$$

$$\eta_{iso} = \frac{(W.D)_{iso}}{(W.D)_{act}}$$

$$\therefore \text{Actual work} = \eta_{mech} \times (W.D)_{theoretical}$$

$$= 0.85 \times 328.66$$

$$(W.D)_{act} = 279.361 \text{ kJ/min}$$

$$\therefore \eta_{iso} = \frac{265.04}{279.361} \times 100$$

$\eta_{iso} = 94.87\%$

11. An air compressor takes in air at 1 bar and 20°C and compresses it according to law $pv^{1.2}=\text{constant}$. It is then delivered to a receiver at a constant pressure of 10 bar. $R=0.287 \text{ kJ/kg K}$. Determine

- (i) Temperature at the end of compression
- (ii) Workdone and heat transferred during compression per kg of air.

Solution

$$T_1=20+273=293 \text{ K}; P_1=1 \text{ bar}; P_2=10 \text{ bar}$$

Law of compression : $pv^{1.2}=C$; $R=287 \text{ J/kgK}$

(i) Temperature at the end of compression T_2

For compression process 1-2, we have

$$\frac{T_2}{T_1} = \left(\frac{P_2}{P_1}\right)^{\frac{n-1}{n}} = \left(\frac{10}{1}\right)^{\frac{1.2-1}{1.2}} = 1.468$$

$$T_2=T_1 \times 1.468 = 293 \times 1.468 = 430 \text{ K or } 157^\circ\text{C}$$

(ii) Workdone and heat transferred during compression per kg of air:

$$\begin{aligned} \text{Workdone, } W &= mRT_1 \frac{n}{n-1} \left[\left(\frac{P_2}{P_1}\right)^{\frac{n-1}{n}} - 1 \right] \\ &= 1 \times 0.287 \times 293 \times \left(\frac{1.2}{1.2-1}\right) \left(\frac{10}{1}\right)^{\frac{1.2-1}{1.2}} - 1 = 236.13 \text{ kJ / kg of air} \end{aligned}$$

Heat transferred during compression,

$$\begin{aligned} Q &= W + \Delta U \\ &= \frac{P_1V_1 - P_2V_2}{n-1} + c_v(T_2 - T_1) = (T_2 - T_1) \left[c_v - \frac{R}{n-1} \right] \\ &= (430-293) \left[0.718 - \frac{0.287}{1.2-1} \right] = -98.23 \text{ kJ/kg} \end{aligned}$$

Negative sign indicates heat rejection.